

Reaktor-Modell - Veresterung

Kurzbeschreibung

Nomenklatur

Stoffdaten

Molmasse:

Uni. Gaskonstante:

$$M_{N_2} := 28.0135 \frac{gm}{mol}$$

Molmasse N2

$$R := 8.314 \frac{J}{mol K}$$

$$M_A := 102.09 \frac{gm}{mol}$$

Molmasse A = Essigsäureanhydrid

$$M_B := 32.04 \frac{gm}{mol}$$

Molmasse B = Methanol

$$M_C := 74.08 \frac{gm}{mol}$$

Molmasse C = Essigsäuremethylester

$$M_D := 60.06 \frac{gm}{mol}$$

Molmasse D = Essigsäure

kritische Daten:

kritische Temperatur

$$T_{krit_A} := 606.05 K$$

$$T_{krit_B} := 513.38 K$$

$$T_{krit_C} := 506.55 K$$

$$T_{krit_D} := 591.95 K$$

kritischer Druck

$$p_{krit_A} := 40 bar$$

$$p_{krit_B} := 82.16 bar$$

$$p_{krit_C} := 47.5 bar$$

$$p_{krit_D} := 57.86 bar$$

kritischer Dichte

$$\rho_{krit_A} := 352 \frac{kg}{m^3}$$

$$\rho_{krit_B} := 282 \frac{kg}{m^3}$$

$$\rho_{krit_C} := 334 \frac{kg}{m^3}$$

$$\rho_{krit_D} := 325 \frac{kg}{m^3}$$

Dichte:

$$\rho_A(Temp) := \text{linterp} \left(\begin{matrix} \begin{bmatrix} \vdots \\ 60 \text{ } ^\circ\text{C} \\ \vdots \end{bmatrix}, \begin{bmatrix} \vdots \\ 1081.719 \frac{kg}{m^3} \\ \vdots \end{bmatrix}, Temp \end{matrix} \right) \text{ Dichte A}$$

$$\rho_B(Temp) := \text{linterp} \left(\begin{matrix} \begin{bmatrix} 0 \text{ } ^\circ\text{C} \\ \vdots \end{bmatrix}, \begin{bmatrix} \vdots \\ 792.033 \frac{kg}{m^3} \\ \vdots \end{bmatrix}, Temp \end{matrix} \right) \text{ Dichte B}$$

$$\rho_C(Temp) := \text{linterp} \left(\begin{matrix} \begin{bmatrix} 0 \text{ } ^\circ\text{C} \\ \vdots \end{bmatrix}, \begin{bmatrix} 968.454 \frac{kg}{m^3} \\ \vdots \end{bmatrix}, Temp \end{matrix} \right) \text{ Dichte C}$$

$$\rho_D(Temp) := \text{linterp} \left(\begin{matrix} \begin{bmatrix} 0 \text{ } ^\circ\text{C} \\ \vdots \end{bmatrix}, \begin{bmatrix} 1059.282 \frac{kg}{m^3} \\ \vdots \end{bmatrix}, Temp \end{matrix} \right) \text{ Dichte D}$$

Verdampfungsenthalpie:

$$\Delta h_{V,A}(Temp) := \text{linterp} \left(\begin{bmatrix} 0 \text{ } ^\circ\text{C} \\ \vdots \end{bmatrix}, \begin{bmatrix} 491852.490 \frac{\text{J}}{\text{kg}} \\ \vdots \end{bmatrix}, Temp \right) \quad \text{Verdampfungsenthalpie A}$$

$$\Delta h_{V,B}(Temp) := \text{linterp} \left(\begin{bmatrix} 0 \text{ } ^\circ\text{C} \\ \vdots \end{bmatrix}, \begin{bmatrix} 1205835.116 \frac{\text{J}}{\text{kg}} \\ \vdots \end{bmatrix}, Temp \right) \quad \text{Verdampfungsenthalpie B}$$

$$\Delta h_{V,C}(Temp) := \text{linterp} \left(\begin{bmatrix} 0 \text{ } ^\circ\text{C} \\ \vdots \end{bmatrix}, \begin{bmatrix} 457174.672 \frac{\text{J}}{\text{kg}} \\ \vdots \end{bmatrix}, Temp \right) \quad \text{Verdampfungsenthalpie C}$$

$$\Delta h_{V,D}(Temp) := \text{linterp} \left(\begin{bmatrix} 0 \text{ } ^\circ\text{C} \\ \vdots \end{bmatrix}, \begin{bmatrix} 393408.254 \frac{\text{J}}{\text{kg}} \\ \vdots \end{bmatrix}, Temp \right) \quad \text{Verdampfungsenthalpie D}$$

Bildungsenthalpien:

$$\Delta H_{B,A} := \frac{-624400 \frac{\text{J}}{\text{mol}}}{M_A} = -6116172.005 \frac{\text{J}}{\text{kg}} \quad \text{Bildungsenthalpie A}$$

$$\Delta H_{B,B} := \frac{-201000 \frac{\text{J}}{\text{mol}}}{M_B} = -6273408.24 \frac{\text{J}}{\text{kg}} \quad \text{Bildungsenthalpie B}$$

$$\Delta H_{B,C} := \frac{-445900 \frac{\text{J}}{\text{mol}}}{M_C} = -6019168.467 \frac{\text{J}}{\text{kg}} \quad \text{Bildungsenthalpie C}$$

$$\Delta H_{B,D} := \frac{-433000 \frac{\text{J}}{\text{mol}}}{M_D} = -7209457.209 \frac{\text{J}}{\text{kg}} \quad \text{Bildungsenthalpie D}$$

$$\Delta H_{B,N_2} := 0 \frac{\text{J}}{\text{kg}} \quad \text{Bildungsenthalpie N}_2$$

Wärmekapazität Flüssigkeit:

$$c_{pL,A}(Temp) := \text{linterp} \left(\begin{bmatrix} 0 \text{ } ^\circ\text{C} \\ \vdots \end{bmatrix}, \begin{bmatrix} 1.726 \frac{\text{J}}{\text{gm K}} \\ \vdots \end{bmatrix}, Temp \right) \quad \text{Wärmekapazität A}$$

$$c_{pL,B}(Temp) := \text{linterp} \left(\begin{bmatrix} 0 \text{ } ^\circ\text{C} \\ \vdots \end{bmatrix}, \begin{bmatrix} 2.403 \frac{\text{J}}{\text{gm K}} \\ \vdots \end{bmatrix}, Temp \right) \quad \text{Wärmekapazität B}$$

$$c_{pL,C}(Temp) := \text{linterp} \left(\begin{bmatrix} 0 \text{ } ^\circ\text{C} \\ \vdots \end{bmatrix}, \begin{bmatrix} 1.826 \frac{\text{J}}{\text{gm K}} \\ \vdots \end{bmatrix}, Temp \right) \quad \text{Wärmekapazität C}$$

$$c_{pL,D}(Temp) := \text{linterp} \left(\begin{bmatrix} 0 \text{ } ^\circ\text{C} \\ \vdots \end{bmatrix}, \begin{bmatrix} 1.931 \frac{\text{J}}{\text{gm K}} \\ \vdots \end{bmatrix}, Temp \right) \quad \text{Wärmekapazität D}$$

Wärmekapazität Gas (isobar):

$$c_{pg,A}(Temp) := \text{linterp} \left(\begin{bmatrix} 0 \text{ } ^\circ\text{C} \\ \vdots \end{bmatrix}, \begin{bmatrix} 0.908 \frac{\text{J}}{\text{gm K}} \\ \vdots \end{bmatrix}, Temp \right) \quad \text{Wärmekapazität A}$$

$$c_{pg,B}(Temp) := \text{linterp} \left(\begin{bmatrix} 0 \text{ } ^\circ\text{C} \\ \vdots \end{bmatrix}, \begin{bmatrix} 1.328 \frac{\text{J}}{\text{gm K}} \\ \vdots \end{bmatrix}, Temp \right) \quad \text{Wärmekapazität B}$$

$$c_{pg,C}(Temp) := \text{linterp} \left(\begin{bmatrix} 0 \text{ } ^\circ\text{C} \\ \vdots \end{bmatrix}, \begin{bmatrix} 1.084 \frac{\text{J}}{\text{gm} \cdot \text{K}} \\ \vdots \end{bmatrix}, Temp \right)$$

Wärmekapazität C

$$c_{pg,D}(Temp) := \text{linterp} \left(\begin{bmatrix} 0 \text{ } ^\circ\text{C} \\ \vdots \end{bmatrix}, \begin{bmatrix} 0.987 \frac{\text{J}}{\text{gm} \cdot \text{K}} \\ \vdots \end{bmatrix}, Temp \right)$$

Wärmekapazität D

$$c_{pg,N2} := 1.040 \frac{\text{J}}{\text{gm} \cdot \text{K}}$$

Wärmekapazität N2

Wärmekapazität Gas (isochor):

$$c_{vg,A}(Temp) := \text{linterp} \left(\begin{bmatrix} 0 \text{ } ^\circ\text{C} \\ \vdots \end{bmatrix}, \begin{bmatrix} 0.908 \frac{\text{J}}{\text{gm} \cdot \text{K}} \\ \vdots \end{bmatrix}, Temp \right) - \frac{R}{M_A}$$

Wärmekapazität A

$$c_{vg,B}(Temp) := \text{linterp} \left(\begin{bmatrix} 0 \text{ } ^\circ\text{C} \\ \vdots \end{bmatrix}, \begin{bmatrix} 1.328 \frac{\text{J}}{\text{gm} \cdot \text{K}} \\ \vdots \end{bmatrix}, Temp \right) - \frac{R}{M_B}$$

Wärmekapazität B

$$c_{vg,C}(Temp) := \text{linterp} \left(\begin{bmatrix} 0 \text{ } ^\circ\text{C} \\ \vdots \end{bmatrix}, \begin{bmatrix} 1.084 \frac{\text{J}}{\text{gm} \cdot \text{K}} \\ \vdots \end{bmatrix}, Temp \right) - \frac{R}{M_C}$$

Wärmekapazität C

$$c_{vg,D}(Temp) := \text{linterp} \left(\begin{bmatrix} 0 \text{ } ^\circ\text{C} \\ \vdots \end{bmatrix}, \begin{bmatrix} 0.987 \frac{\text{J}}{\text{gm} \cdot \text{K}} \\ \vdots \end{bmatrix}, Temp \right) - \frac{R}{M_D}$$

Wärmekapazität D

$$c_{vg,N2}(Temp) := c_{pg,N2} - \frac{R}{M_{N2}} = 0.743 \frac{\text{J}}{\text{gm} \cdot \text{K}}$$

Wärmekapazität N2

Dampfdruck:

| Parameter A | Parameter B | Parameter C | Parameter D |
|------------------------|------------------------|------------------------|------------------------|
| $A_{ps,A} := -8.15436$ | $A_{ps,B} := -8.72963$ | $A_{ps,C} := -8.57584$ | $A_{ps,D} := -9.34304$ |
| $B_{ps,A} := 1.80785$ | $B_{ps,B} := 1.4586$ | $B_{ps,C} := 4.22791$ | $B_{ps,D} := 3.77735$ |
| $C_{ps,A} := -3.76039$ | $C_{ps,B} := -2.78449$ | $C_{ps,C} := -5.37346$ | $C_{ps,D} := -3.59092$ |
| $D_{ps,A} := -3.04616$ | $D_{ps,B} := -0.70669$ | $D_{ps,C} := -0.82045$ | $D_{ps,D} := -1.57006$ |

$$p_{s,A}(Temp) := p_{krit,A} \cdot e^{\left(\frac{T_{krit,A}}{Temp} \cdot \left(A_{ps,A} \cdot \left(1 - \frac{Temp}{T_{krit,A}} \right) + B_{ps,A} \cdot \left(1 - \frac{Temp}{T_{krit,A}} \right)^{1.5} + C_{ps,A} \cdot \left(1 - \frac{Temp}{T_{krit,A}} \right)^{2.5} + D_{ps,A} \cdot \left(1 - \frac{Temp}{T_{krit,A}} \right)^5 \right) \right)}$$

$$p_{s,B}(Temp) := p_{krit,B} \cdot e^{\left(\frac{T_{krit,B}}{Temp} \cdot \left(A_{ps,B} \cdot \left(1 - \frac{Temp}{T_{krit,B}} \right) + B_{ps,B} \cdot \left(1 - \frac{Temp}{T_{krit,B}} \right)^{1.5} + C_{ps,B} \cdot \left(1 - \frac{Temp}{T_{krit,B}} \right)^{2.5} + D_{ps,B} \cdot \left(1 - \frac{Temp}{T_{krit,B}} \right)^5 \right) \right)}$$

$$p_{s,C}(Temp) := p_{krit,C} \cdot e^{\left(\frac{T_{krit,C}}{Temp} \cdot \left(A_{ps,C} \cdot \left(1 - \frac{Temp}{T_{krit,C}} \right) + B_{ps,C} \cdot \left(1 - \frac{Temp}{T_{krit,C}} \right)^{1.5} + C_{ps,C} \cdot \left(1 - \frac{Temp}{T_{krit,C}} \right)^{2.5} + D_{ps,C} \cdot \left(1 - \frac{Temp}{T_{krit,C}} \right)^5 \right) \right)}$$

$$p_{s,D}(Temp) := p_{krit,D} \cdot e^{\left(\frac{T_{krit,D}}{Temp} \cdot \left(A_{ps,D} \cdot \left(1 - \frac{Temp}{T_{krit,D}} \right) + B_{ps,D} \cdot \left(1 - \frac{Temp}{T_{krit,D}} \right)^{1.5} + C_{ps,D} \cdot \left(1 - \frac{Temp}{T_{krit,D}} \right)^{2.5} + D_{ps,D} \cdot \left(1 - \frac{Temp}{T_{krit,D}} \right)^5 \right) \right)}$$

Kinetik

Geschw.koeffizient:

$$k_{0,1}(x) := -1.36 \cdot 10^8 \frac{\text{L}}{\text{mol s}} + 1.36 \cdot 10^8 \cdot \exp(2.2 \cdot x) \cdot \frac{\text{L}}{\text{mol s}}$$

$$k_{0,2}(x) := 2 \cdot 10^7 \cdot \exp(-12.28 \cdot x) \cdot \frac{\text{L}^2}{\text{mol}^2 \text{ s}}$$

Aktivierungsenergie:

$$E_{A,1}(x) := -15924 \cdot x^2 \frac{\text{J}}{\text{mol}} + 20568 \cdot x \frac{\text{J}}{\text{mol}} + 77337 \frac{\text{J}}{\text{mol}}$$

$$E_{A,2}(x) := -40472 \cdot x \frac{\text{J}}{\text{mol}} + 80750 \frac{\text{J}}{\text{mol}}$$

Reaktionsenthalpie:

$$\Delta H_R := -66300 \frac{\text{J}}{\text{mol}} = -66300 \frac{\text{J}}{\text{mol}}$$

Prozessdaten

Referenztemperatur:

$$T_{ref} := 298.15 \text{ K}$$

Referenzdruck:

$$p_{ref} := 1 \text{ bar}$$

Dosierstrom:

$$m_{B,F} := 0 \frac{\text{kg}}{\text{s}}$$

Dosiertemperatur:

$$T_{B,F} := 80 \text{ °C}$$

Berechnung des Anfangszustand im Reaktor pT-Flash

pT-Flash --> Druck und Temperatur sind bekannt und konstant. Gesucht ist die Zusammensetzung der Flüssigkeit und Gasphase bzw. ihre Massen je Komponente.

$$pT_Flash(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) := \left| \begin{array}{l} x_{spec,A} \leftarrow \frac{\frac{m_{0,A}}{M_A}}{\frac{m_{0,A}}{M_A} + \frac{m_{0,B}}{M_B} + \frac{m_{0,C}}{M_C} + \frac{m_{0,D}}{M_D}} \\ x_{spec,B} \leftarrow \frac{\frac{m_{0,B}}{M_B}}{\frac{m_{0,A}}{M_A} + \frac{m_{0,B}}{M_B} + \frac{m_{0,C}}{M_C} + \frac{m_{0,D}}{M_D}} \\ m_{0,C} \end{array} \right|$$

$$x_{spec_C} \leftarrow \frac{\frac{m_{0_C}}{M_C}}{\frac{m_{0_A}}{M_A} + \frac{m_{0_B}}{M_B} + \frac{m_{0_C}}{M_C} + \frac{m_{0_D}}{M_D}}$$

$$x_{spec_D} \leftarrow \frac{\frac{m_{0_D}}{M_D}}{\frac{m_{0_A}}{M_A} + \frac{m_{0_B}}{M_B} + \frac{m_{0_C}}{M_C} + \frac{m_{0_D}}{M_D}}$$

$$p_{sat_A} \leftarrow p_{s_A}(Temp)$$

$$p_{sat_B} \leftarrow p_{s_B}(Temp)$$

$$p_{sat_C} \leftarrow p_{s_C}(Temp)$$

$$p_{sat_D} \leftarrow p_{s_D}(Temp)$$

$$p_{spec} \leftarrow x_{spec_A} \cdot p_{sat_A} + x_{spec_B} \cdot p_{sat_B} + x_{spec_C} \cdot p_{sat_C} + x_{spec_D} \cdot p_{sat_D}$$

for $i \in 0 \dots 100$

$$m_l \leftarrow \frac{m_{0_A} + m_{0_B} + m_{0_C} + m_{0_D} - \frac{Vol}{R \cdot Temp} (x_{spec_A} \cdot p_{sat_A} \cdot M_A + x_{spec_B} \cdot p_{sat_B} \cdot M_B + x_{spec_C} \cdot p_{sat_C} \cdot M_C + x_{spec_D} \cdot p_{sat_D} \cdot M_D)}{1 - \frac{1}{R \cdot Temp} (x_{spec_A} \cdot M_A + x_{spec_B} \cdot M_B + x_{spec_C} \cdot M_C + x_{spec_D} \cdot M_D) \cdot \left(\frac{x_{spec_A} \cdot M_A}{\rho_A(Temp)} + \frac{x_{spec_B} \cdot M_B}{\rho_B(Temp)} + \frac{x_{spec_C} \cdot M_C}{\rho_C(Temp)} + \frac{x_{spec_D} \cdot M_D}{\rho_D(Temp)} \right) \cdot (x_{spec_A} \cdot p_{sat_A} \cdot M_A + x_{spec_B} \cdot p_{sat_B} \cdot M_B + x_{spec_C} \cdot p_{sat_C} \cdot M_C + x_{spec_D} \cdot p_{sat_D} \cdot M_D)}$$

$$V_l \leftarrow \frac{m_l}{x_{spec_A} \cdot M_A + x_{spec_B} \cdot M_B + x_{spec_C} \cdot M_C + x_{spec_D} \cdot M_D} \cdot \left(\frac{x_{spec_A} \cdot M_A}{\rho_A(Temp)} + \frac{x_{spec_B} \cdot M_B}{\rho_B(Temp)} + \frac{x_{spec_C} \cdot M_C}{\rho_C(Temp)} + \frac{x_{spec_D} \cdot M_D}{\rho_D(Temp)} \right)$$

$$V_g \leftarrow Vol - V_l$$

$$m_{g_A} \leftarrow \frac{x_{spec_A} \cdot p_{sat_A} \cdot V_g \cdot M_A}{R \cdot Temp}$$

$$m_{g_B} \leftarrow \frac{x_{spec_B} \cdot p_{sat_B} \cdot V_g \cdot M_B}{R \cdot Temp}$$

$$m_{g_C} \leftarrow \frac{x_{spec_C} \cdot p_{sat_C} \cdot V_g \cdot M_C}{R \cdot Temp}$$

$$m_{g_D} \leftarrow \frac{x_{spec_D} \cdot p_{sat_D} \cdot V_g \cdot M_D}{R \cdot Temp}$$

$$m_{g_N2} \leftarrow \frac{(p_{spec} - x_{spec_A} \cdot p_{sat_A} - x_{spec_B} \cdot p_{sat_B} - x_{spec_C} \cdot p_{sat_C} - x_{spec_D} \cdot p_{sat_D}) \cdot V_g \cdot M_{N2}}{R \cdot Temp}$$

$$m_g \leftarrow m_{g_N2} + m_{g_A} + m_{g_B} + m_{g_C} + m_{g_D}$$

$$m_{l_A} \leftarrow m_{0_A} - m_{g_A}$$

$$m_{l_B} \leftarrow m_{0_B} - m_{g_B}$$

$$m_{l_C} \leftarrow m_{0_C} - m_{g_C}$$

$$m_{l_D} \leftarrow m_{0_D} - m_{g_D}$$

$$x_{spec_A} \leftarrow \frac{\frac{m_{l_A}}{M_A}}{\frac{m_{l_A}}{M_A} + \frac{m_{l_B}}{M_B} + \frac{m_{l_C}}{M_C} + \frac{m_{l_D}}{M_D}}$$

$$x_{spec_B} \leftarrow \frac{\frac{m_{l_B}}{M_B}}{\frac{m_{l_A}}{M_A} + \frac{m_{l_B}}{M_B} + \frac{m_{l_C}}{M_C} + \frac{m_{l_D}}{M_D}}$$

$$x_{spec_C} \leftarrow \frac{\frac{m_{l_C}}{M_C}}{\frac{m_{l_A}}{M_A} + \frac{m_{l_B}}{M_B} + \frac{m_{l_C}}{M_C} + \frac{m_{l_D}}{M_D}}$$

$$x_{spec_D} \leftarrow \frac{\frac{m_{l_D}}{M_D}}{\frac{m_{l_A}}{M_A} + \frac{m_{l_B}}{M_B} + \frac{m_{l_C}}{M_C} + \frac{m_{l_D}}{M_D}}$$

$$y_{spec_A} \leftarrow \frac{\frac{m_{g_A}}{M_A}}{\frac{m_{g_A}}{M_A} + \frac{m_{g_B}}{M_B} + \frac{m_{g_C}}{M_C} + \frac{m_{g_D}}{M_D} + \frac{m_{g_N2}}{M_{N2}}}$$

$$\begin{aligned}
 & \begin{matrix} \text{---A} & \text{---B} & \text{---C} & \text{---D} & \text{---N}_2 \\ & & \frac{m_{g,B}}{M_B} & & \\ y_{spec,B} \leftarrow & \frac{m_{g,A}}{M_A} + \frac{m_{g,B}}{M_B} + \frac{m_{g,C}}{M_C} + \frac{m_{g,D}}{M_D} + \frac{m_{g,N_2}}{M_{N_2}} & & & \\ & & \frac{m_{g,C}}{M_C} & & \\ y_{spec,C} \leftarrow & \frac{m_{g,A}}{M_A} + \frac{m_{g,B}}{M_B} + \frac{m_{g,C}}{M_C} + \frac{m_{g,D}}{M_D} + \frac{m_{g,N_2}}{M_{N_2}} & & & \\ & & \frac{m_{g,D}}{M_D} & & \\ y_{spec,D} \leftarrow & \frac{m_{g,A}}{M_A} + \frac{m_{g,B}}{M_B} + \frac{m_{g,C}}{M_C} + \frac{m_{g,D}}{M_D} + \frac{m_{g,N_2}}{M_{N_2}} & & & \\ & & \frac{m_{g,N_2}}{M_{N_2}} & & \\ y_{spec,N_2} \leftarrow & \frac{m_{g,A}}{M_A} + \frac{m_{g,B}}{M_B} + \frac{m_{g,C}}{M_C} + \frac{m_{g,D}}{M_D} + \frac{m_{g,N_2}}{M_{N_2}} & & & \\ p_{spec} \leftarrow & x_{spec,A} \cdot p_{sat,A} + x_{spec,B} \cdot p_{sat,B} + x_{spec,C} \cdot p_{sat,C} + x_{spec,D} \cdot p_{sat,D} + \frac{m_{g,N_2} \cdot R \cdot Temp}{V_g \cdot M_{N_2}} & & & \\ \left[x_{spec,A} & x_{spec,B} & x_{spec,C} & x_{spec,D} & y_{spec,A} & y_{spec,B} & y_{spec,C} & y_{spec,D} & y_{spec,N_2} & m_l & m_g & V_l & V_g & p_{spec} \right]^T
 \end{matrix}
 \end{aligned}$$

Startzusammensetzung Flüssigkeit:

$$x_{0,A}(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) := pT_Flash(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D})_0$$

$$x_{0,B}(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) := pT_Flash(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D})_1$$

$$x_{0,C}(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) := pT_Flash(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D})_2$$

$$x_{0,D}(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) := pT_Flash(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D})_3$$

Startzusammensetzung Gas:

$$y_{0,A}(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) := pT_Flash(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D})_4$$

$$y_{0,B}(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) := pT_Flash(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D})_5$$

$$y_{0,C}(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) := pT_Flash(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D})_6$$

$$y_{0,D}(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) := pT_Flash(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D})_7$$

$$y_{0,N_2}(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) := pT_Flash(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D})_8$$

Startmassen und Startvolumen:

$$m_{0,l}(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) := pT_Flash(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D})_9$$

$$m_{0,g}(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) := pT_Flash(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D})_{10}$$

$$m_0(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) := m_{0,l}(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) + m_{0,g}(Vol, Temp, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D})$$

$$m_{0_g_N2}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) := m_{0_g}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) \cdot \zeta_{0_g_N2}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D})$$

$$m_{0_A}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) := m_{0_l_A}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) + m_{0_g_A}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D})$$

$$m_{0_B}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) := m_{0_l_B}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) + m_{0_g_B}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D})$$

$$m_{0_C}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) := m_{0_l_C}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) + m_{0_g_C}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D})$$

$$m_{0_D}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) := m_{0_l_D}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) + m_{0_g_D}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D})$$

$$x_0(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) := \frac{\frac{m_{0_l_A}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D})}{M_A}}{\frac{m_{0_l_A}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D})}{M_A} + \frac{m_{0_l_B}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D})}{M_B}}$$

Innere Energien zum Startzeitpunkt:

$$h_{0_l}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) := \zeta_{0_l_A}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) \downarrow$$

- $(\Delta H_{B_A} + c_{pl_A}(Temp) \cdot (Temp - T_{ref}) - \Delta h_{V_A}(Temp)) \downarrow$
- + $\zeta_{0_l_B}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) \downarrow$
- $(\Delta H_{B_B} + c_{pl_B}(Temp) \cdot (Temp - T_{ref}) - \Delta h_{V_B}(Temp)) \downarrow$
- + $\zeta_{0_l_C}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) \downarrow$
- $(\Delta H_{B_C} + c_{pl_C}(Temp) \cdot (Temp - T_{ref}) - \Delta h_{V_C}(Temp)) \downarrow$
- + $\zeta_{0_l_D}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) \downarrow$
- $(\Delta H_{B_D} + c_{pl_D}(Temp) \cdot (Temp - T_{ref}) - \Delta h_{V_D}(Temp)) \downarrow$

$$h_{0_g}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) := \zeta_{0_g_A}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) \downarrow$$

- $(\Delta H_{B_A} + c_{pg_A}(Temp) \cdot (Temp - T_{ref})) \downarrow$
- + $\zeta_{0_g_B}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) \downarrow$
- $(\Delta H_{B_B} + c_{pg_B}(Temp) \cdot (Temp - T_{ref})) \downarrow$
- + $\zeta_{0_g_C}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) \downarrow$
- $(\Delta H_{B_C} + c_{pg_C}(Temp) \cdot (Temp - T_{ref})) \downarrow$
- + $\zeta_{0_g_D}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) \downarrow$
- $(\Delta H_{B_D} + c_{pg_D}(Temp) \cdot (Temp - T_{ref})) \downarrow$
- + $\zeta_{0_g_N2}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) \downarrow$
- $(\Delta H_{B_N2} + c_{pg_N2} \cdot (Temp - T_{ref})) \downarrow$

$$H_0(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) := h_{0_l}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) \cdot m_{0_l}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) \downarrow$$

$$+ h_{0_g}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) \cdot m_{0_g}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D})$$

$$U_0(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) := H_0(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) \downarrow$$

$$- p_0(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D}) \cdot Vol$$

| | |
|---|------|
| | Temp |
| $p_0(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D})$ | |
| | Vol |
| $V_{0_l}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D})$ | |
| $V_{0_g}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D})$ | |
| $x_{0_A}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D})$ | |
| $x_{0_B}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D})$ | |
| $x_{0_C}(Vol, Temp, m_{0_A}, m_{0_B}, m_{0_C}, m_{0_D})$ | |

$$\text{Startbed}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) := \begin{bmatrix}
 x_{0,D}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 y_{0,A}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 y_{0,B}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 y_{0,C}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 y_{0,D}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 y_{0,N2}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 m_0(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 m_{0,l}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 m_{0,g}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 \zeta_{0,l,A}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 \zeta_{0,l,B}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 \zeta_{0,l,C}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 \zeta_{0,l,D}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 \zeta_{0,g,A}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 \zeta_{0,g,B}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 \zeta_{0,g,C}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 \zeta_{0,g,D}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 \zeta_{0,g,N2}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 m_{0,l,A}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 m_{0,l,B}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 m_{0,l,C}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 m_{0,l,D}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 m_{0,g,A}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 m_{0,g,B}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 m_{0,g,C}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 m_{0,g,D}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 m_{0,g,N2}(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 m_{0,A} \\
 m_{0,B} \\
 m_{0,C} \\
 m_{0,D} \\
 U_0(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D}) \\
 x_0(\text{Vol}, \text{Temp}, m_{0,A}, m_{0,B}, m_{0,C}, m_{0,D})
 \end{bmatrix}$$

Uvm-Flash

DGL-System für Reaktor

Startmasse im Reaktor Komponente:

$$m_{1,A} := 0.051 \text{ kg} \quad m_{1,B} := 0.006408 \text{ kg} \quad m_{1,C} := 0 \text{ kg} \quad m_{1,D} := 0 \text{ kg}$$

Starttemperatur:

$$T_1 := 66 \text{ }^\circ\text{C}$$

Reaktorvolumen:

$$V_1 := 0.07 \text{ L}$$

Startzeit, Endzeit, Schrittlänge, Schrittzahl, Kinetikparameter:

$$t_{start_1} := 0 \text{ s} \quad t_{end_1} := 15 \text{ min} \quad \Delta t_1 := 0.01 \text{ min} \quad n_1 := \frac{t_{end_1} - t_{start_1}}{\Delta t_1} = 1500$$

Startmasse im Reaktor Komponente:

$$m_{2,A} := 0.04915 \text{ kg} \quad m_{2,B} := 0.03085 \text{ kg} \quad m_{2,C} := 0 \text{ kg} \quad m_{2,D} := 0 \text{ kg}$$

Starttemperatur:

$$T_2 := 24.5 \text{ }^\circ\text{C}$$

Reaktorvolumen:

$$V_2 := 0.11 \text{ L}$$

Startzeit, Endzeit, Schrittlänge, Schrittzahl, Kinetikparameter:

$$t_{start_2} := 0 \text{ s} \quad t_{end_2} := 166 \text{ min} \quad \Delta t_2 := 0.01 \text{ min} \quad n_2 := \frac{t_{end_2} - t_{start_2}}{\Delta t_2} = 16600$$

Startmasse im Reaktor Komponente:

$$m_{3,A} := 0.03656 \text{ kg} \quad m_{3,B} := 0.02302 \text{ kg} \quad m_{3,C} := 0 \text{ kg} \quad m_{3,D} := 0 \text{ kg}$$

Starttemperatur:

$$T_3 := 24.75 \text{ }^\circ\text{C}$$

Reaktorvolumen:

$$V_3 := 0.082 \text{ L}$$

Startzeit, Endzeit, Schrittlänge, Schrittzahl, Kinetikparameter:

$$t_{start_3} := 0 \text{ s} \quad t_{end_3} := 166 \text{ min} \quad \Delta t_3 := 0.01 \text{ min} \quad n_3 := \frac{t_{end_3} - t_{start_3}}{\Delta t_3} = 16600$$



$$t_{start_1} \quad t_{end_1} \quad \Delta t_1$$

$$x_1 := Startbed(V_1, T_1, m_{1_A}, m_{1_B}, m_{1_C}, m_{1_D})_{40} = 0.714$$

$$\begin{bmatrix} m_{l_A1} \\ \vdots \end{bmatrix} := Lsg(V_1, T_1, m_{1_A}, m_{1_B}, m_{1_C}, m_{1_D}, x_1, t_{end_1}, n_1)$$

Startmasse im Reaktor Komponente:

$$m_{4_A} := 6.0586 \text{ kg} \quad m_{4_B} := 1.9014 \text{ kg} \quad m_{4_C} := 0 \text{ kg} \quad m_{4_D} := 0 \text{ kg}$$

Starttemperatur:

$$T_4 := 29.5 \text{ }^\circ\text{C}$$

Reaktorvolumen:

$$V_4 := 10 \text{ L}$$

Startzeit, Endzeit, Schrittlänge, Schrittzahl, Kinetikparameter:

$$t_{start_4} := 0 \text{ s} \quad t_{end_4} := 93 \text{ min} \quad \Delta t_4 := 0.001 \text{ min} \quad n_4 := \frac{t_{end_4} - t_{start_4}}{\Delta t_4} = 93000$$

$$x_4 := Startbed(V_4, T_4, m_{4_A}, m_{4_B}, m_{4_C}, m_{4_D})_{40} = 0.5$$

$$\begin{bmatrix} m_{l_A4} \\ \vdots \end{bmatrix} := Lsg(V_4, T_4, m_{4_A}, m_{4_B}, m_{4_C}, m_{4_D}, x_4, t_{end_4}, n_4)$$

$$t_{start_2} \quad t_{end_2} \quad \Delta t_2$$

$$x_2 := Startbed(V_2, T_2, m_{2_A}, m_{2_B}, m_{2_C}, m_{2_D})_{40} = 0.333$$

$$\begin{bmatrix} m_{l_A2} \\ \vdots \end{bmatrix} := Lsg(V_2, T_2, m_{2_A}, m_{2_B}, m_{2_C}, m_{2_D}, x_2, t_{end_2}, n_2)$$

Startmasse im Reaktor Komponente:

$$m_{5_A} := 0.4918 \text{ kg} \quad m_{5_B} := 0.3078 \text{ kg} \quad m_{5_C} := 0 \text{ kg} \quad m_{5_D} := 0 \text{ kg}$$

Starttemperatur:

$$T_5 := 15.5 \text{ }^\circ\text{C}$$

Reaktorvolumen:

$$V_5 := 1 \text{ L}$$

Startzeit, Endzeit, Schrittlänge, Schrittzahl, Kinetikparameter:

$$t_{start_5} := 0 \text{ s} \quad t_{end_5} := 316 \text{ min} \quad \Delta t_5 := 0.001 \text{ min} \quad n_5 := \frac{t_{end_5} - t_{start_5}}{\Delta t_5} = 316000$$

$$x_5 := Startbed(V_5, T_5, m_{5_A}, m_{5_B}, m_{5_C}, m_{5_D})_{40} = 0.334$$

$$\begin{bmatrix} m_{l_A5} \\ \vdots \end{bmatrix} := Lsg(V_5, T_5, m_{5_A}, m_{5_B}, m_{5_C}, m_{5_D}, x_5, t_{end_5}, n_5)$$

$$t_{start_3} \quad t_{end_3} \quad \Delta t_3$$

$$x_3 := Startbed(V_3, T_3, m_{3_A}, m_{3_B}, m_{3_C}, m_{3_D})_{40}$$

$$\begin{bmatrix} m_{l_A3} \\ \vdots \end{bmatrix} := Lsg(V_3, T_3, m_{3_A}, m_{3_B}, m_{3_C}, m_{3_D}, x_3, t_{end_3}, n_3)$$

Informationen

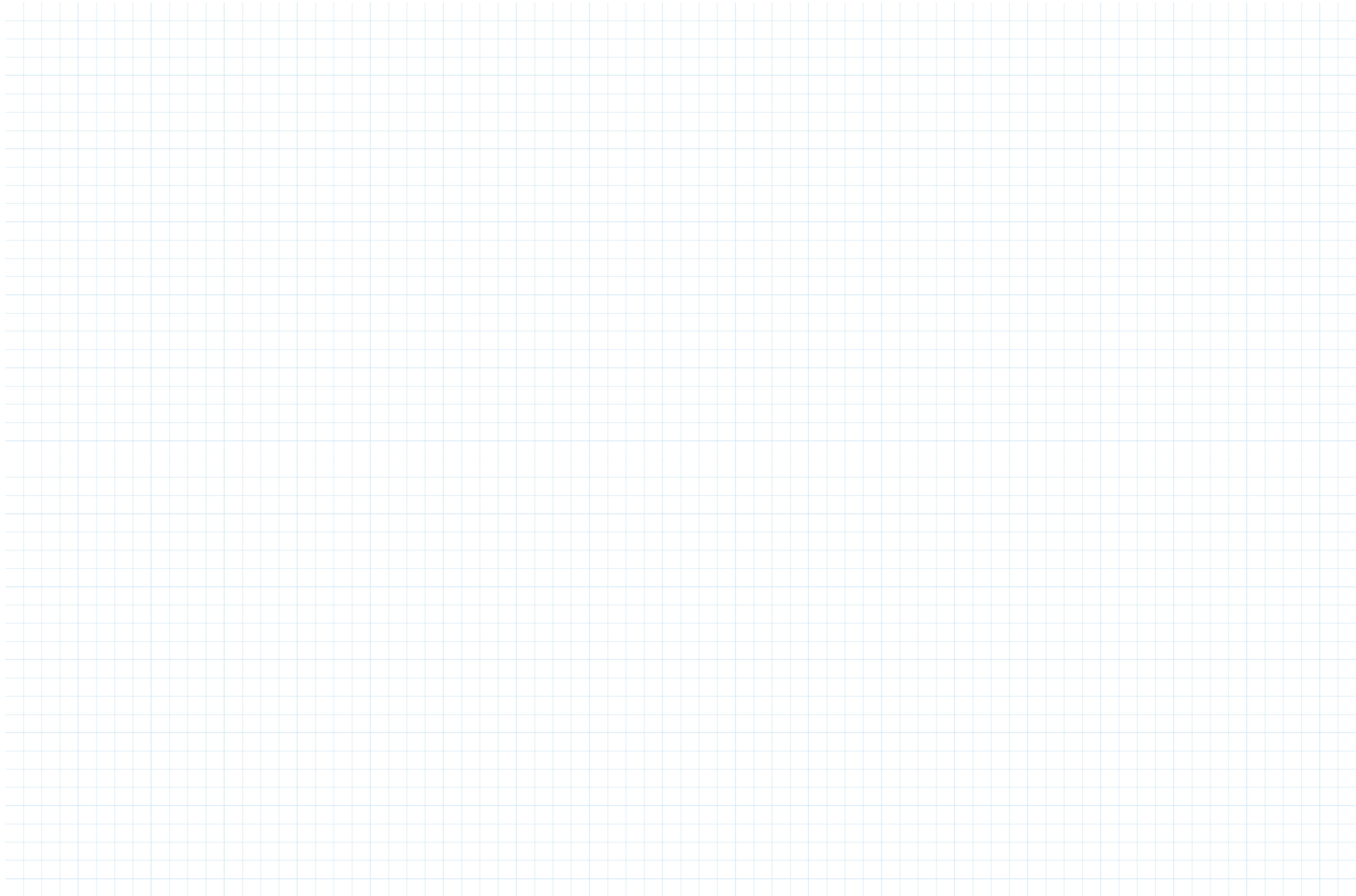
CSE Institut | Joseph-von-Fraunhofer Str. 9 | D-76327 PFINZTAL

Reaktor_Ester_v2.7.mcdx

02.03.2018

Fabian Görlich

Projekt





$$time := t_{start} \cdot \Delta t \cdot 100 \cdot t_{prozess} = ?$$

$$time1 := \text{READExcel}("C:\Users\fago\Desktop\Projekt_Ester\Messdaten\Messdaten_Modelldaten.xlsx", "[4]A8:A43") \cdot 1 \text{ s} = ?$$

$$time2 := \text{READExcel}("C:\Users\fago\Desktop\Projekt_Ester\Messdaten\Messdaten_Modelldaten.xlsx", "[4]C8:C43") \cdot 1 \text{ s} = ?$$



Eingaben

$excel_{\text{"Tabelle1!A1"}} := \text{"Zeit (s)"} \quad excel_{\text{"Tabelle1!B1"}} := \text{"Temperatur (°C)"} \quad excel_{\text{"Tabelle1!C1"}} := \text{"Zeit (s)"} \quad excel_{\text{"Tabelle1!D1"}} := \text{"Druck (bar)"} \quad excel_{\text{"Tabelle1!A2"}} := \text{time1} \quad excel_{\text{"Tabelle1!B2"}} := T(\text{time1}) - 273.15 \text{ K} \quad excel_{\text{"Tabelle1!C2"}} := \text{time1} \quad excel_{\text{"Tabelle1!D2"}} := p(\text{time1}) \cdot 10^{-5}$

| Zeit (s) | Temperatur | Zeit (s) | Druck (bar) |
|-----------|------------|-----------|-------------|
| 10,220418 | 26,8703889 | 16,04344 | 0,12721022 |
| 97,86583 | 27,0789387 | 177,71196 | 0,12864044 |
| 231,05971 | 27,2288661 | 291,25015 | 0,12967699 |
| 375,2955 | 27,3884872 | 409,7248 | 0,13078829 |
| 509,86896 | 27,5549058 | 530,66766 | 0,13195544 |

Ausgaben